# Status Update on PR1410 – Hydrogen Fluoride Storage and Use at Petroleum Refineries



# SCAQMD REFINERY COMMITTEE

January 20, 2018
Torrance, California

## PUBLIC PROCESS

- Six working group meetings conducted since April 2017
- Presentations provided:
  - Refineries' Current Mitigations
  - CEC's Potential Transportation Fuel Supply and Price Impacts of HF Ban
  - API RP 751 Safe Operation of Hydrofluoric Acid (HF) Alkylation Units
  - Alternative Alkylation Technologies (DuPont/CB&I/Chevron)
  - Cal-OSHA Process Safety Management Regulation
  - TRAA's Modified HF (MHF)/HF Alkylation Dangers
  - SCAQMD's Proposed Rule Concepts
- Five technical discussion meetings with Torrance Refining Company (TORC)
- Two refinery site visits & Torrance refinery community/neighborhood tour
- Interagency meeting with US EPA and Cal-OSHA

## GENESIS OF PR1410 RULEMAKING

- "Near-miss" accident at Torrance refinery on February 18, 2015
- Community concerns on the alkylation unit safety, potential HF release and corresponding risk
- Hazards and human health risk due to exposure to HF are greater than those of sulfuric acid
- Additional information made available
  - More studies and documentation on MHF
  - Viable alternative technologies have matured and are being implemented
- SCAQMD staff conducted independent assessment

## HF

Sulfuric Acid

Appearance

Vapor Density

**Boiling Point** 

Hazards

Rate of Onset

Isolating Distance\*

Colorless, fuming liquid/gas

0.7 (relative to air)

67 °F

Severe skin and deep tissue burns, changing the bone structure

Immediate & delayed

At least 330 ft.

Colorless, oily liquid

3.4 (relative to air)

554 °F

Severe irritation and skin burn, carcinogenic

**Immediate** 

At least 150 ft.

<sup>\*</sup> Isolate leak area in all directions as an immediate precautionary measure (source: https://cameochemicals.noaa.gov)

## "NEAR-MISS" ACCIDENT



Each settler tank contains 47,000 lb of MHF



## ASSESSMENT OF MHF TECHNOLOGY

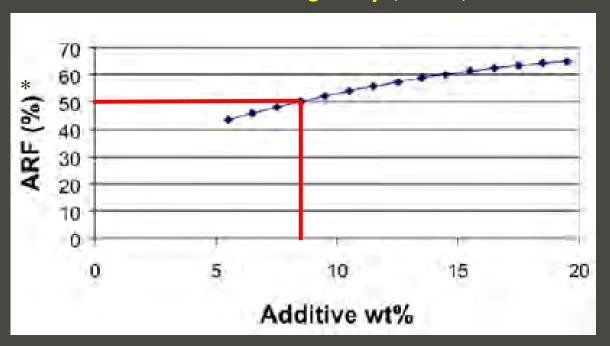
- Staff has assessed the scientific information provided by TORC on MHF
- Assessing the safety of MHF technology is very complex and uncertainty still exists
- Summary results of MHF assessment:
  - $\square$  Some, but uncertain, HF mitigation benefits offered by MHF (< 35%)
  - Ability to prevent formation of vapor/aerosol cloud is uncertain.
    - ✓ Conditions of testing are different from current operating conditions
    - ✓ Large hole sizes were not considered
  - □ Ignoring all the uncertainties, best case scenario with all existing mitigation measures added at TORC, HF reduction is 89% leaving 11% released
- In case of breach in one settler tank at TORC, potential release of 5,200 lb HF assuming all passive mitigation functioning properly

## HF REDUCTION BENEFITS OFFERED BY MHF

#### Lab Tests and Modeling

#### (100% SULFOLANE) (30%)80 (50%)(40%) 70 RAINOUT **Best Case** 50 ~35% %t% $(\sim 10\%)$ benefit • (20%) 30 20 10 100 200 300 400 500 600 700 800 900 1000 1100 1200 1300 VAPOR PRESSURE, mm Hg

#### **Modeling Only (TORC)**



(SCAQMD Meeting MHF Technology Discussion with TORC, May 4, 2017)

<sup>\*</sup> Airborne Reduction Factor

## INITIAL RULE CONCEPTS

- HF mitigation tiered at three different levels and with different timeline
  - □ Tier | Mitigation Require existing mitigation with some enhancements
  - □ Tier | Mitigation Above and beyond Tier | Mitigation (API recommendations)
  - Tier III Mitigation Greatly enhanced protection (failsafe systems)
- Option to change to alternative technologies in lieu of Tier II and/or Tier III Mitigation

## TIER I MITIGATION

- HF point sensors
- Alarm set points
- Open path monitors 4 sided
   (TORC and/or Valero would need to install)
- Video cameras + monitor screens in remote control room
- HF sensitive paint
- Water mitigation
   (TORC would need to install water curtain)
- Acid evacuation system

- Emergency isolation block valves
- Backup power
- Baffles

(TORC would need to install)

- Acid settler pans
- Flange shrouds

(Valero would need to install)

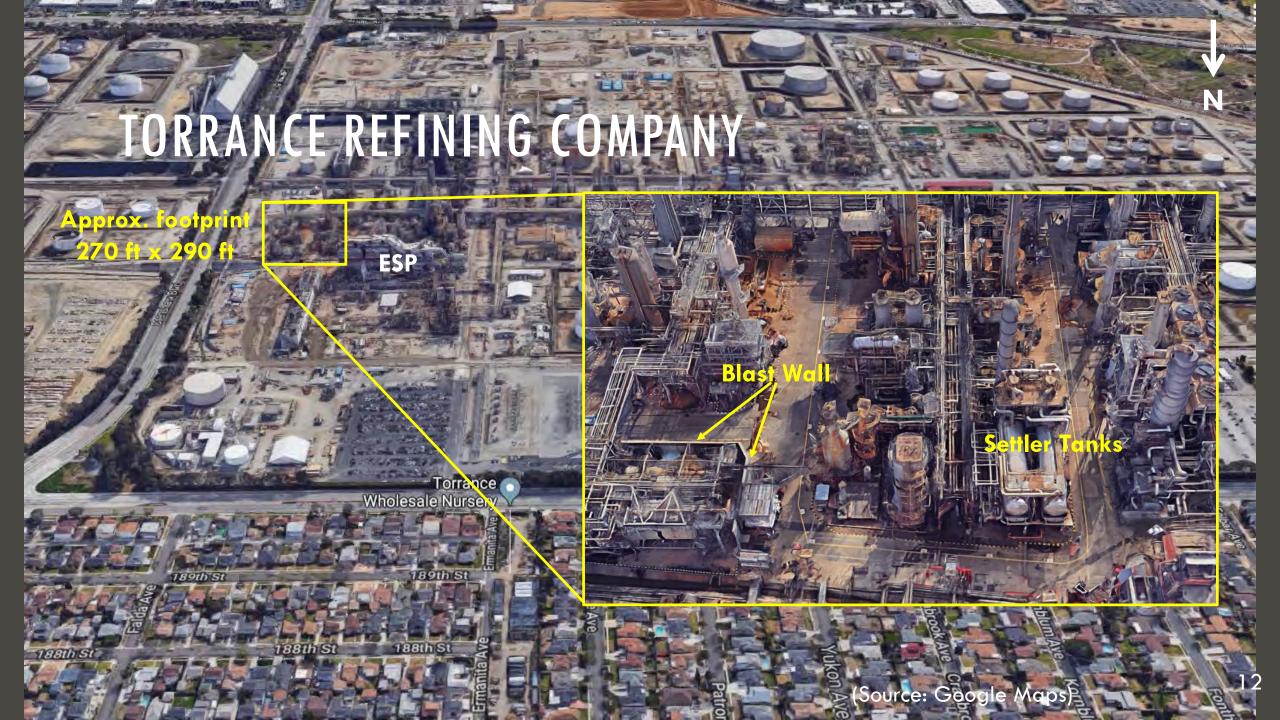
- Pump barriers
- Safety audits

## TIER II MITIGATION

- Automated systems (water mitigation, emergency block valves) at alarm set points of HF sensors & open path monitors
- State-of-the-art high definition cameras (increase number of cameras & monitors)
- More HF sensors to compensate for non-operating sensors
- More comprehensive barriers (e.g., enclosure around acid settler tanks)
- ✓ Cost Range: \$50 \$100 MM

## TIER III MITIGATION (POTENTIAL APPROACHES)

- Complete, full enclosure of alkylation unit with roll-up doors, comprehensive water spray (worker safety), sensors & drainage capabilities
  - Possibly build whole new containment system parallel to existing unit to reduce downtime
  - Need to address potential "unintended secondary consequences" (e.g., flammable gases)
- Negatively pressured enclosure venting to scrubber with drainage
- Fully automated systems including acid evacuation at alarm set points
- Underground storage (acid dump tank, fresh storage, etc.)
- $\checkmark$  Cost Range: \$50 − \$150 MM (based on chlorine gas containment and handling facility)





## COMPARISON OF ALTERNATIVES TO HF

| Catalyst Type                     | Sulfuric Acid   |   | Solid Acid   | Ionic Liquid   |
|-----------------------------------|---|---|--|--|
| Technology Name<br>(Manufacturer) | CDAlky®<br>(CB&I)   | ConvEx <sup>SM</sup><br>(DuPont/STRATCO)          | AlkyClean®<br>(CB&I)   | ISOALKY™<br>(Chevron & UOP)  |
| Cost                              | Less than conventional sulfuric acid unit (30–50% less acid consumption)                                    | ~40–60% less than a grassroots sulfuric acid unit | Information not available  | Information not available  |
| Associated Hazards                | Sulfuric acid   | Sulfuric acid                                     | No known hazards   | No known hazards   |
| Commercial Applications/Status    | One US Gulf Coast refinery start-up in 2020 at comparable capacity (23,000 b/d) and 13 refineries worldwide | None, new technology                              | Petrochemical plant in<br>China at lower<br>capacity (2,700 b/d) | Chevron Salt Lake City HF alkylation retrofit, with planned start-up in 2020 at lower capacity (5,000 b/d) |

# EXISTING COST ANALYSIS OF TECHNOLOGY CONVERSION

### Conversion to sulfuric acid

| Cost Range       | Conditions   | Reference                 |
|------------------|--|---------------------------|
| \$100 - \$200 MM | US Gulf Coast cost; Alkylation unit only   | Norton Engineering (2016) |
| \$210 - \$330 MM | US Gulf Coast & Midwest costs;<br>Alkylation unit (~23,000 b/d)<br>and acid regeneration | DuPont<br>(2018)          |
| \$600 – \$900 MM | TORC cost; Alkylation unit and acid regeneration   | Burns & McDonnell (2017)  |

# POTENTIAL TIMING FOR IMPLEMENTATION

- 2018 Rule adoption
- 6-12 months after adoption Require Tier I Mitigation measures
- 2-3 years after adoption Require Tier II Mitigation or alternative technology
- 2021 Alternative technology assessment completed
- 8 years after adoption Require Tier III Mitigation or alternative technology